



Extraction of humic acids and their fractions in poly (ethylene glycol)-based aqueous biphasic systems

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Received 8 May 2001; received in revised form 27 September 2001; accepted 27 September 2001

Abstract

The possibility of extraction and fractionation of humic acid (HA) in the aqueous biphasic system (ABS) was shown for the first time. The 10% PEG–10% (NH₄)₂SO₄–H₂O and 5% PEG–7.5% dextran (or dextran sulphate, sodium salt)–H₂O systems were used. HA originated from peat, soddy-podzolic soil and chernozem were studied. The distribution coefficients were measured for HA of different origin, size of the molecules, molecular weight (MW) of the polymers and pH of the system. The PEG–(NH₄)₂SO₄–H₂O system was found to be better for preconcentration and isolation of HA, whereas the PEG–dextran–H₂O system is preferable for HA fractionation. The extractability of HA in ABS increases with increasing the MW of HA molecules. Peat HA are extracted in ABS with higher distribution coefficients compared with chernozem and soddy-podzolic soil HA. It is consistent with higher hydrophobicity of peat HA revealed by hydrophobic interaction chromatography. ABS are promising for HA separation into fractions that differ in their hydrophobic/hydrophilic properties as well as for comparing HA of different origin by their relative hydrophobicity. © 2001 Published by Elsevier Science B.V.

Keywords: Humic acids; Aqueous biphasic systems; Fractionation; Membrane filtration; Gel permeation chromatography

1. Introduction

Humic substance (HS) are natural organic compounds ubiquitous in soils, sediments and waters. They are formed in the process of humification from different structural precursors of biotic origin and have irregular structure and varying composition [1,2]. Generally HS can be described as a complex mixture of related polyelectrolyte-like macromolecules which differ in chemical composition and size. Because of the heterogeneity and polydispersity of HS their molecular

structure is not well understood yet, however, it is generally accepted that they consist of aromatic rings and aliphatic chains which carry O-, N- and S-containing functional groups [1,3].

Due to a broad spectrum of polar groups and non-polar fragments HS interact with metal ions, minerals and organic compounds [4–6], thus playing an important role in soil formation processes and binding of environmental pollutants. For better understanding of the mechanisms of these reactions and predicting the HS behaviour in natural processes, more detailed information is needed about molecules, structural constituents and groupings involved, as well as about their complexing capabilities. For such

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49 complex mixtures as HS their better characterisation
50 can hardly be achieved without application of frac-
51 tionation techniques based on different properties of
52 the macromolecules.

53 A traditional fractionation method applied to HS
54 is based on their separation into humic acid (HA)
55 and fulvic acid (FA) according to different solubil-
56 ities of HS components in acidic medium. HA are
57 soluble in alkali but precipitated at pH 1–2, while
58 FA are soluble in both alkaline and acidic aqueous
59 solutions.

60 Various other separation procedures have been
61 employed for HS: gel permeation chromatography
62 (GPC), membrane filtration (MF) to fractionate HS
63 by their size (molecular weight (MW)) [7–9]; elec-
64 trophoresis to separate HS on the basis of their size and
65 charge [10,11]; hydrophobic interaction chromatog-
66 raphy to obtain distribution patterns of hydrophobic
67 and hydrophilic fragments of HS [12]. Combinations
68 of various fractionation and extraction methods pro-
69 vide more complete information about HS and their
70 fractions which can have different properties, e.g.
71 different complexing abilities [13].

72 Liquid–liquid extraction is one of the most useful
73 techniques for the recovery, separation and investiga-
74 tion of organic and inorganic substances. However,
75 hydrophilic HS are poorly extracted to conventional
76 organic solvents in traditional oil/water systems. We
77 have suggested that HS should be better extracted
78 in aqueous polymer-based two-phase systems. Such
79 aqueous biphasic system (ABS) have been success-
80 fully used in biotechnology for the fractionation of cell
81 particles and macromolecules [14,15], for analytical
82 and radiochemical separations of metal ions as their
83 complexes with inorganic ligands and water-soluble
84 organic reagents [15–19], but have never been applied
85 to extracting HS.

86 Biphasic systems can be obtained by mixing aque-
87 ous solutions of two dissimilar polymers or of a poly-
88 mer and an inorganic salt. Usually two-phase aque-
89 ous systems are prepared on the basis of poly(ethylene
90 glycol) (PEG), which is salted out from a solution of
91 inorganic salt or another polymer and forms a separate
92 top phase. Both PEG-rich and bottom phases contain
93 significant amounts of water (80–90%), that reduces
94 the effect of hydration on the transfer of the compound
95 to be extracted from one phase to another. This al-
96 lows one to separate strongly hydrated species whose

extraction in traditional solvent extraction systems is 97
difficult or impossible. 98

99 Separation of macromolecules in ABS is based
100 mainly on their different hydrophilic/hydrophobic
101 properties. Due to water structuring near the poly-
102 mer chains, hydrophobic interactions between
103 –CH₂–CH₂– groups of PEG and non-polar groups
104 of the extracted organic macromolecules are entropy
105 favourable. The presence of aromatic structures, ac-
106 cessible to hydrophobic interactions, is important
107 because purely aliphatic organic molecules are poorly
108 extracted to the PEG-rich phase.

109 The distribution of a biomolecule between two
110 phases in ABS is characterised by distribution coef-
111 ficient (*D*). It is dependent on different parameters of
112 extraction system as well as on the size of macro-
113 molecules, their charge and conformation, which
114 determine the type and number of groups accessible
115 to the solvent molecules [14].

116 In our investigations, we used aqueous systems of
117 PEG–ammonium sulphate, PEG–dextran sulphate,
118 sodium salt (NaSD), and PEG–dextran which provide
119 rather high rates of phase separation. The distribution
120 coefficients were measured for HA of different origin,
121 size of the molecules, MW of the polymers and pH
122 of the system.

2. Experimental 123

2.1. Reagents 124

125 The following chemicals were used in the ex-
126 periments: NaOH, HCl, NaCl, KCl, (NH₄)₂SO₄,
127 (NH₄)₂Cr₂O₇ (Reakhim, Russia); Tris (Reanal, Hun-
128 gary); sodium dodecyl sulphate (SDS) (Serva, Ger-
129 many); Blue dextran 2000 (Pharmacia, Sweden); PEG
130 with MW of 4, 6, 12 and 20 kDa (Loba Chemie,
131 Germany); dextran T70 and T500 with MW of 70
132 and 500 kDa, respectively (Loba Chemie, Germany);
133 NaSD with a MW of 500 kDa (Pharmacia Fine Chem-
134 icals, Sweden). Aqueous solutions of all reagents were
135 prepared using Milli-Q (Millipore) distilled water.

2.2. Extraction and preparation of humic acid 136

137 HA from peat (HA_p, “Merck” preparation), soddy-
138 podzolic soil (HA_s) and chernozem (HA_{ch}) were stud- 138

139 ied. HS were leached by aqueous 0.1 M NaOH solu- 183
140 tion from A1 horizons of respective soils using the 184
141 conventional procedure [20]. HA were precipitated 185
142 from the obtained extract by its acidification to pH 186
143 1–2 by concentrated HCl. Then HA were purified by 187
144 salting-out with 0.4 M NaCl solution in water and gel 188
145 filtration on a 1.0 cm × 26 cm column (Pharmacia, 189
146 Sweden) filled with Sephadex G-10 gel as described 190
147 elsewhere [21]. 191

148 2.3. Size fractionation of humic acid 192 149 by GPC and MF 193

150 High- and low-MW fractions of HA_p were obtained 196
151 by GPC on a K 2.6 cm × 70 cm column (Pharmacia, 197
152 Sweden), filled with Sephadex G-75 gel (Pharmacia 198
153 Fine Chemicals, Sweden) using 0.05 M NaOH as the 199
154 eluent at a flow rate of 20 ml h⁻¹. Then the HA were 200
155 precipitated from the obtained solutions by HCl to 201
156 adjust pH <2 and air dried. 202

157 Samples of HA_p (0.5 mg ml⁻¹ in 0.05 M Tris–HCl 203
158 buffer, pH 8.2) were also fractionated using an on-line 204
159 multi-stage MF device (OMFD-2) [22]. The total 205
160 inner volume of the device is 15 ml, it contains five 206
161 polymethacrylate discs having non-spiral channels in 207
162 the upper part and bearing 47 mm Millipore poly- 208
163 sulphone membranes with pore sizes of 0.45, 0.1, 209
164 0.05, 0.03 and 0.005 μm; 15 ml of 0.05 M Tris–HCl 210
165 buffer were pumped through the device (at a pres- 211
166 sure of 2.5 bar) and after that the sample was passed 212
167 through. Portions of liquid fractions from every fil- 213
168 tration stage were taken after obtaining 30 ml of 214
169 the filtrate. 215

170 2.4. Characterisation of humic acid 216

171 The elemental composition was determined on a 217
172 CHNS analyser “Karlo-Erba” 1106 (*t* = 1000 °C). 218
173 UV–VIS spectra of HA solutions (pH 12) were 219
174 recorded on a Shimadzu UV-2501 PC spectropho- 220
175 tometer. 221

176 The distribution of hydrophobic and hydrophilic 222
177 fragments in HA was estimated on a 1.0 cm × 10 cm 223
178 column (Amicon) filled with octyl-Sepharose CL-4B 224
179 gel (Pharmacia, Sweden). The elution was carried out 225
180 at a rate of 10 ml h⁻¹, firstly in 0.05 M Tris–HCl buffer 226
181 and after that in 0.05 M Tris–HCl + 0.3% SDS buffer 227
182 with a step buffer change gradient. 228

The molecular weight distributions of unfraction- 183
ated and MF-fractionated HA were obtained on a 184
K 0.9 cm × 60 cm column (Pharmacia, Sweden) 185
filled with Sephadex G-100 gel (eluent: 0.025 M 186
Tris–HCl buffer + 0.05 M NaCl + 0.1% SDS, elution 187
rate 3 ml h⁻¹). The elution profiles were recorded at 188
280 nm using a 2238 UVICORD SII detector (LKB, 189
Sweden). The MW distributions of HA fraction- 190
ated by GPC were obtained on a K 1.6 cm × 70 cm 191
column (Pharmacia, Sweden) filled with Sephadex 192
G-75 gel (eluent: 0.025 M Tris–HCl buffer + 0.05 M 193
NaCl + 0.1% SDS, elution rate 3 ml h⁻¹). Each 194
column was calibrated by Blue dextran 2000 and 195
(NH₄)₂Cr₂O₇ solutions in the eluent buffer to de- 196
termine a column void volume and a total gel bed 197
volume, respectively. 198

There are no proper of HA-like substances with de- 199
fined MW that could be used as standards for accurate 200
MW determination. We had to calculate the average 201
MW of HA using the Determan’s empirical formula 202
for globular proteins [23] 203

$$\text{Sephadex G – 75 gel : } \log \text{ MW} = 5.624 - 0.752 \frac{V_e}{V_0} \quad 204$$

$$\text{Sephadex G – 100 gel : } \log \text{ MW} = 5.941 - 0.847 \frac{V_e}{V_0} \quad 205$$

where MW is molecular weight, *V*₀ the column void 206
volume and *V*_e is the elution volume, each measured 207
from the start of the sample application to the centre 208
of elution peak. 209

210 2.5. Preparation of aqueous biphasic system 216

The 10% PEG–10% (NH₄)₂SO₄–HA–H₂O systems 211
were prepared by mixing 1 ml of 30% PEG solution 212
(pH 3.5) with 1 ml of 30% solution of ammonium sul- 213
phate (pH 5.6) and 1 ml of HA (2 mg ml⁻¹ in 0.05 M 214
NaOH). The systems of 5% PEG–7.5% dextran (or 215
NaSD)–HA–H₂O were prepared by mixing 0.5 ml of 216
30% PEG with 1.5 ml of 15% solution of the second 217
polymer (pH 7.0) and 1 ml of 2 mg ml⁻¹ solution of 218
HA or its fraction, obtained by GPC. Solutions of HA 219
fractionated by MF were taken just from the OMFD-2 220
reservoirs. NaCl was added to the PEG–NaSD–H₂O 221
system to adjust an ionic strength of 0.3. The mixtures 222
were shaken for 1 min. After complete phase separa- 223
tion for an hour aliquots were taken from each phase 224

225 and diluted by 10 times in KCl–NaOH buffer (pH 12).
 226 Then the absorbances at 465 nm were measured on a
 227 SF-46 spectrophotometer (LOMO, Russia). The dis-
 228 tribution coefficients were calculated as following:

$$229 D = \frac{\text{absorbance at 465 nm of the top (PEG – rich) phase}}{\text{absorbance at 465 nm of the bottom phase}}$$

230 The pH-dependence of HA distribution was studied
 231 using a PEG 12000–dextran 70000 aqueous system.
 232 A set of two-phase systems was prepared where pH
 233 at equilibrium varied from 4 to 12.1 (pH was adjusted
 234 by 0.3 M HCl). The pH values were measured using a
 235 pH meter Horiba F-16 with a combined electrode of
 236 Horiba 6367-10D.

237 3. Results and discussion

238 3.1. Characterisation of humic acid

239 The HA elemental composition and E values (ab-
 240 sorbance of 0.001% HA solution at 465 or 650 nm, pH
 241 12) are shown in Table 1. With a certain approxima-
 242 tion, H:C ratios can be used to assess a contribution
 243 of aliphatic chains bearing $\equiv\text{CH}$, $=\text{CH}_2$, $-\text{CH}_3$ groups
 244 to the HA structure. The H:C ratio is highest for HA_p
 245 which may contain the largest number of aliphatic
 246 fragments among the studied HA, while HA_{ch} is most
 247 aromatic. The UV–VIS spectra obtained were typi-
 248 cal for HA and had no maxima except for HA_s spec-
 249 tra where a shoulder in the region of 440–480 nm
 250 and small maxima at 575 and 620 nm were observed.
 251 These maxima are usually attributed to the presence
 252 of green P_g pigment, commonly found in preparations
 253 of HA originated from soddy-podzolic soils [1]. The
 254 E values increased in the order $\text{HA}_s < \text{HA}_p < \text{HA}_{ch}$.
 255 Highest E values were found for HA_{ch} that is in agree-

256 ment with elemental analysis data, suggesting that this
 257 HA is most aromatic.

258 The reversed-phase hydrophobic interaction chro-
 259 matography (RPHIC) profiles are shown in Fig. 1.
 260

261 RPHIC is based on the distribution of organic
 262 molecules between a liquid polar mobile phase and a
 263 non-polar stationary phase (hydrophobic gel matrix).
 264 The larger the content of hydrophobic fragments of
 265 the molecules, the stronger is their affinity to the
 266 hydrophobic matrix. Molecules are eluted from the
 267 column in the order of their hydrophobicity. Deter-
 268 gents are often added to the mobile phase to elute
 269 most hydrophobic molecules. Thus, RPHIC permits
 270 to separate organic molecules according to their rel-
 271 ative hydrophobicity. It should be noted that the
 272 distribution profiles in RPHIC are highly dependent
 273 on the matrix and eluent used. Therefore, the dis-
 274 tribution patterns obtained are valid for operational
 275 experimental conditions.

276 HA macromolecules are amphiphilic, i.e. they con-
 277 tain both hydrophobic and hydrophilic fragments.
 278 Hydrophilic fragments are represented by O- and
 279 N-containing polar groups. The hydrophobicity of
 280 HA may be due to the presence of aromatic structures
 281 (for example, aromatic rings) and non-polar aliphatic
 282 chains [1]. The molecules containing a larger number
 283 of hydrophilic fragments were eluted first from the
 284 column (Fig. 1). More hydrophobic HA molecules
 285 were stronger retained by the hydrophobic matrix
 286 and eluted after addition of an ionic detergent (SDS)
 287 to the eluent. Assuming that the absorbances of hy-
 288 drophobic and hydrophilic fractions were the same
 289 for all HA studied, the relative hydrophobicity of HA
 290 was estimated taking into consideration the corre-

Table 1
 Elemental composition of humic acids and their UV–VIS data

HA	Content (at.%)				Atomic ratios			UV–VIS data	
	C	H	O ^a	N	H:C	O:C	N:C	E_{450}	$E_{450}:E_{650}$
HA_p	35.9	40.7	21.7	1.7	1.13	0.60	0.05	0.051	3.9
HA_s	37.3	41.3	18.7	2.7	1.12	0.50	0.07	0.043	4.3
HA_{ch}	41.8	35.3	19.7	3.2	0.84	0.47	0.08	0.070	3.8

^a O content is found from the difference.

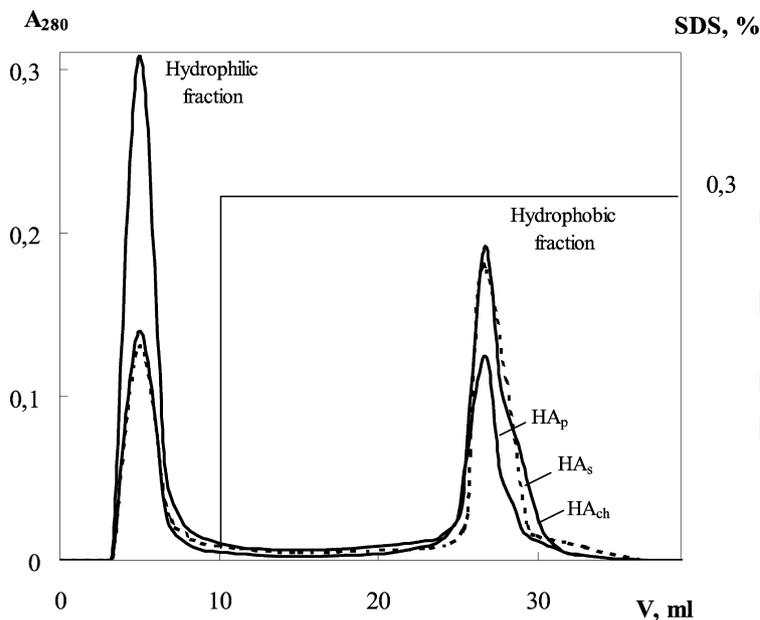


Fig. 1. Reversed-phase hydrophobic interaction chromatography profiles of humic acids. Column 1.0 cm \times 10 cm, octyl-Sepharose CL-4B gel, elution by 0.05 M Tris-HCl buffer and after that by 0.05 M Tris-HCl + 0.3% SDS buffer with a step buffer change gradient, flow rate 10 ml h⁻¹.

291 sponding peak areas in the chromatograms. The ratios
 292 between the areas of hydrophobic and hydrophilic
 293 peaks for peat, soddy-podzolic soil and chernozem
 294 HA were 1.5, 1.0 and 0.7, respectively, thus HA_p is
 295 most “hydrophobic” among the studied HA.

296 Gel-chromatographic profiles of HA consist of three
 297 fractions (Fig. 2): a high molecular weight (HMW)
 298 fraction eluted in a void volume (MW > 150 kDa),
 299 a middle molecular weight (MMW) fraction (MW
 300 60–72 kDa) and a low molecular weight (LMW) frac-
 301 tion (MW 6–10 kDa).

302 The percentage of each fraction in HA (percentage
 303 of total chromatogram area) was calculated taking
 304 into consideration the corresponding peak areas in
 305 gel-chromatograms. The peak areas of HMW and
 306 LMW fractions were obtained by multiplying the
 307 squares of segments A and B by a factor of two, re-
 308 spectively (Fig. 3). The peak area of MMW frac-
 309 tion was found by difference between the total chro-
 310 matogram area and the areas for HMW and LMW
 311 fractions. The results are presented in Table 2. The
 312 LMW fraction is of the largest content in all HA stud-
 313 ied. The mean MW of this fraction is highest for HA_p.

3.2. Size fractionation of humic acid

314 GPC was used to obtain HMW and LMW fractions
 315 of HA_p. The MW of HMW fraction eluted in a void
 316 volume was >75 kDa. The average MW of LMW frac-
 317 tion was about 5 kDa.

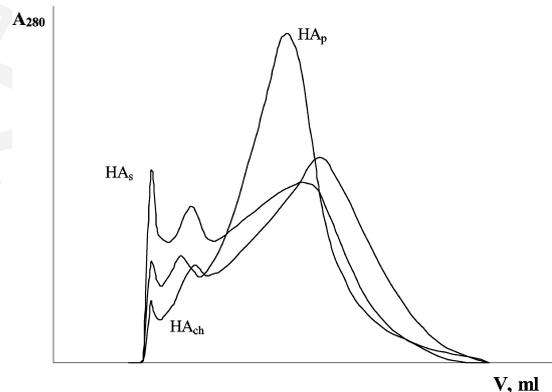


Fig. 2. Gel-chromatographic profiles of humic acids. Column K 0.9 cm \times 60 cm, Sephadex G-100 gel, elution by 0.025 M Tris-HCl (pH 8.2) + 0.05 M NaCl + 0.1% SDS buffer, flow rate 3 ml h⁻¹.

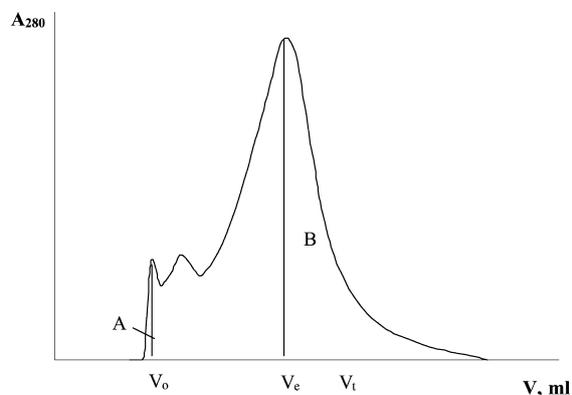


Fig. 3. Gel-chromatographic profile of peat HA. The elution peak areas of high and low molecular weight fractions were obtained by multiplying by a factor of 2 the squares of segments A and B, respectively. The peak area of middle molecular weight fraction is found by difference.

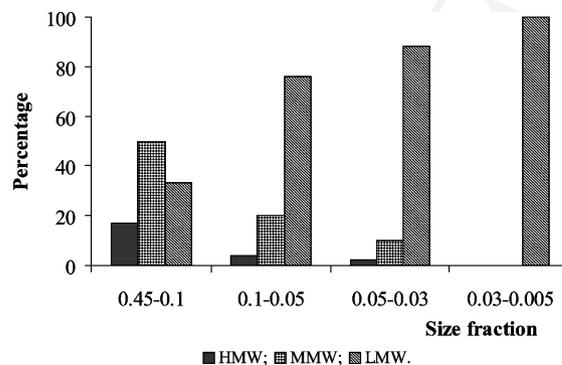


Fig. 4. Percentage of high, middle and low molecular weight fractions in MF-fractionated HA samples.

318 Peat HA was also fractionated by MF. A filtrate obtained with a starting membrane (0.45 μm) was further fractionated with membranes of decreasing pore sizes down to 0.005 μm. The HA molecules, which are able to penetrate all the membranes used, are found in the filtrate of the last membrane. Each HA fraction obtained by the MF procedure contain not only molecules passed through a certain membrane but also molecules from further filtration steps.

327 The molecular sizes between 0.005 and 0.45 μm are roughly within an HS MW from $<10^3$ to $>10^6$ kDa [9]. More detailed information about the molecular size distribution of HA in MF filtrates can be provided by GPC. The gel-chromatographic profiles of 0.45–0.1 and 0.1–0.05 μm HA samples consisted of three fractions: HMW eluted in a void volume (MW > 150 kDa), shoulder-like MMW (62 kDa) and LMW

(5 kDa). The percentage of each fraction observed in the gel-chromatograms was calculated according to the procedure described above (Fig. 3). The results are shown in Fig. 4. It can be seen from the figure that the 0.1–0.45 μm size fraction contains about 17% of HMW molecules. The HA fractions with molecular sizes of 0.03–0.05 and 0.005–0.03 μm contain 88 and 100% of LMW molecules, respectively. Thus, with decreasing the membrane pore size the percentage of LMW molecules increases in the respective filtrates (size fractions).

3.3. Fractionation of humic acid in ABS

347 Concentrations of the polymers necessary for the formation of two phases were chosen on the basis of phase diagrams [14]. A diagram for the PEG 6000–dextran 500000 system is shown in Fig. 5.

351 The bold curve represents a binodal below which the system is homogeneous. The straight line connecting points B and C is tie line. Point A characterises the initial composition of the whole system chosen for our studies, points B and C characterise the individual compositions of top and bottom phases after phase separation. The approximate phase volume ratio can be estimated by segments AB and AC [14]. It can be seen from Fig. 3 that although each phase contains certain amounts of both polymers, the bottom phase is enriched by dextran and the top phase is enriched by PEG. The binodal position depends on the type of polymer, its concentration and MW, temperature, pH and other variables.

Table 2

Average molecular weights (kDa) and relative contents (%) of fractions in HA

HA	Fraction 1		Fraction 2		Fraction 3	
	MW	Content	MW	Content	MW	Content
HA _p	>150	4	72	14	10	82
HA _s	>150	7	72	31	8	62
HA _{ch}	>150	2	60	16	6	82

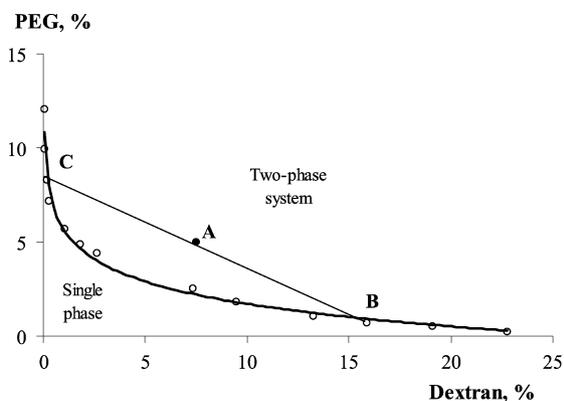


Fig. 5. Phase diagram of the PEG 6000–dextran 500000–H₂O system. Point A characterises the initial composition of the whole system, points B and C characterise the individual compositions of top and bottom phases after phase separation. The approximate phase volume ratio is estimated by segments AB and AC.

365 The results presented in Table 3 show that HA can
 366 be extracted in ABS. At pH about 12 the distribution
 367 coefficients are higher than unity and much higher than
 368 those in HA extraction in traditional oil/water systems.
 369 This is most probably due to hydrophobic interactions
 370 between non-polar fragments of HA molecules and
 371 –CH₂–CH₂– groups of the linear polyether molecules.
 372 It is important that the presence of polar and dissoci-
 373 ated groups in HA molecules does not impair the ex-
 374 traction that is the principal difference of ABS from
 375 traditional water-organic solvent systems.

The *D* values are maximum for the PEG–(NH₄)₂SO₄–H₂O system and the distribution coefficients for the PEG–NaSD–H₂O system are somewhat higher than for the PEG–dextran–H₂O system. The relative hydrophobicity of phases in polymeric systems studied decreases in the order [14]

PEG > dextran > NaSD > (NH₄)₂SO₄

Thus, top and bottom phases of the PEG–(NH₄)₂SO₄–H₂O system are most contrast by their hydrophobic properties, comparing with other systems under study. This can serve as an explanation why HA are extracted with highest *D* values in this system, while the distribution of HA in more “soft” two-polymer-based systems is more uniform.

Thus, one can operate either with hard or soft systems depending on the problem to be solved. The PEG–(NH₄)₂SO₄–H₂O system best suits for preconcentration and isolation of HA, whereas the PEG–dextran–H₂O system is better for HA fractionation.

Relationships between the MW of the polymers and the distribution coefficients for HA have also been studied. No effect of MW has been found for the PEG–(NH₄)₂SO₄–H₂O system within the studied range of PEG MW (from 4 to 20 kDa). The systems based on two polymers exhibit more narrow heterogeneity regions than the PEG–salt–H₂O system [18]. With decreasing the PEG MW, the binodial for a two-polymer system shifts upward and the equilibrium composition of the two phases become closer to

Table 3
Distribution coefficients of HA in ABS

HA	PEG, MW (kDa)	PEG–(NH ₄) ₂ SO ₄	PEG–dextran T70	PEG–dextran T500	PEG–NaSD
HA _s	20	4.4	–	–	9.5
	12	5.5	2.7	4.0	3.6
	6	3.5	1.4	2.3	–
	4	4.3	–	No phase separation	–
HA _{ch}	20	5.0	–	–	16.4
	12	4.4	2.6	4.2	4.8
	6	5.5	1.2	1.9	–
	4	3.8	–	No phase separation	–
HA _p	20	18.8	–	–	16.9
	12	17.0	3.5	5.2	4.3
	6	21.0	2.0	2.8	–
	4	11.1	–	No phase separation	–

Table 4
Distribution coefficients for GPC-fractionated HA_p in PEG–dextran 70000–H₂O system

Sample	PEG 12000	PEG 20000
LMW	2.1	2.8
HMW	5.7	10.6

each other at a given initial composition of the system. This might be a reason for more uniform distribution of the solute between the two phases and consequently for lower D values (Table 3). At as low PEG MW as 4 kDa, the two-polymer systems are homogeneous at the chosen concentrations of the components.

The data on the extraction of GPC-fractionated HA in PEG–dextran 70000–H₂O systems show that the D values are higher for the HMW fraction (Table 4). This can be due to higher relative hydrophobicity of the HMW fraction. The results of extraction of MF-fractionated HA in the same ABS are presented in Table 5. It can be seen from this table that the overall tendency remains the same: the distribution coefficients are higher for HMW fractions.

Of three HA studied, the highest distribution coefficients were obtained for HA_p. The other two HA had similar D values. It was interesting to compare these results with those obtained by GPC and RPHIC. It was shown that the larger the average MW of the compound under study the higher is its distribution coefficient in ABS (Tables 4 and 5). The LMW fraction was of the largest content in all HA studied, and its average MW was highest for HA_p (Table 2). This may explain a better extractability of HA_p in the ABS. According to the RPHIC data (Fig. 1), HA_p are most hydrophobic that is a reason for better transfer to the more hydrophobic PEG-rich phase.

Table 5
Distribution coefficients for MF-fractionated HA_p in PEG–dextran 70000–H₂O system

MW of PEG (kDa)	Size of the fractions (μm)			
	0.45–0.1	0.1–0.05	0.05–0.03	0.03–0.005
12	2.5	1.5	1.7	1.1
20	7.9	3.6	4.1	1.9

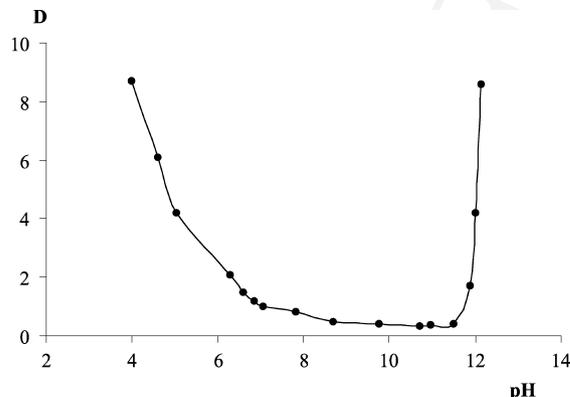


Fig. 6. Dependence of HA_p distribution on equilibrium pH for 5% PEG–7.5% dextran 70000–H₂O system.

Finally, pH-dependence of HA distribution in ABS was studied. It can be seen from Fig. 6 that the relationship is rather complicated. The D values decrease from 8.7 to 0.35 with pH increasing from 4 to 11. Further increase in pH leads to a drop in the D values (to 8.6 at pH 12.1). The preferential transfer of HA to the PEG-rich phase at lower pH values could be explained by suppressed ionisation of functional groups in acidic medium and conformational changes of HA molecules. However, it is difficult to interpret a sharp increase in D values on going from pH 11.5 to 12. Further studies are needed to understand such a complicated pH-dependence.

4. Conclusions

The principal difference of ABS from traditional water–organic solvent extraction systems, is that they enable to achieve the extraction and separation of strongly hydrated molecules of HA, containing polar and dissociated groups. The extraction of HA to any organic solvents in conventional liquid–liquid systems is difficult or impossible. Compared to other HA fractionation techniques the new approach proposed is rather simple, time saving, and cheap. Extracted HA can be easily separated from the polymers by either precipitation with concentrated HCl or filtration through Sephadex G-10 gel. It is recommended to use the extraction in ABS in combination with other techniques for fractionation and characterisation of HA.

463 **Acknowledgements**

464 The authors are grateful to the Russian Founda-
465 tion for Basic Research (projects nos. 99-03-32653,
466 99-04-48007 and 01-04-06107) for support of this
467 work.

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